Contact Mechanics and Elements of Tribology Lecture 7. Lubrication and Sealing

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Outline

1 Lubrication

- Regimes of lubrication
- Derivation of the Reynolds equation
- Analytical solution for hydrostatic lubrication in bearings
- Elasto-hydrodynamic lubrication
- 2 Sealing
 - Metal-to-metal face seal for nuclear power plant applications
 - Fluid-structure coupling
 - Results of FE numerical simulation

Acknowledgment:

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Lubrication: what is it?

- Lubrication: technique to reduce friction and wear between relatively moving surfaces by adding a solid/liquid/gas lubricant
- Studied in Tribology (Greek: tribo -"to rub", logy - "study of")
 'The Jost Report' (1966): cost of friction, wear and corrosion to UK economy P. Jost (1966)



Lubricant over gears www.iselinc.com

- Applications:
 - gears
 - bearings

- seals - cams
- ngs
- piston heads
- metal forming - HDD ...
- human joints
- Recent report (2017):
 23% of total world energy losses come from tribological contacts (20% friction, 3% wear)

K. Holmberg, A. Erdemir, Friction (2017)



Lubricating a bike chain www.madegood.org

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Lubricant over gears www.efficientplantmag.com

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- seals
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- camsmetal forming
- piston heads - human joints
- HDD ...
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Lubricated roller bearing www.bearingtips.com

Lubrication regimes: Stribeck curve



Hydrodynamic lubrication (HL)

- Conforming surfaces
- No elastic effect
- Normal load fully supported by thin fluid film
- $\bullet h_{\min} = f(P, U, \eta, R)$
- $p \le 5$ MPa, $h_{\min} > 1 \ \mu m$

 Mechanism of pressure development in fluid film:









Squeeze film bearing



Externally pressurized bearing

Newtonian fluid

 Viscous stresses in flowing fluid are linearly proportional to the strain rate - the gradient of the velocity:

$$\tau = \eta \frac{\partial u}{\partial z}$$

- *τ* is the shear stress in the fluid
- η is the viscosity (absolute, or dynamic) of the fluid
- $\frac{\partial u}{\partial y}$ is the shear strain rate
- In general 3D case for arbitrary coordinate system:

$$\tau_{ij} = \eta \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$



Petrov's equation

Shear stress:

$$\tau = \eta \frac{\partial u}{\partial z} = \eta \frac{U}{h}$$

Frictional reaction:

$$T = A\tau = (2\pi rb)\,\eta \frac{U}{h}$$

The coefficient of friction:

$$\mu = \frac{T}{P} = \frac{2\pi r b}{h} \frac{\eta U}{P}$$





Stresses on the surface of a fluid element



Stresses on the surface of a fluid element:

$$\tau_{ij} = \eta \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right), \quad \tau_{ij} = \tau_{ji}$$

$$\sigma_i = -p - \frac{2}{3}\eta \nabla \cdot \underline{u} + 2\eta \frac{\partial u_i}{\partial x_i}$$

- η absolute viscosity
- *p* hydrostatic pressure
- x_i coordinates
- *u_i* velocity componets
- g acceleration of gravity

Navier-Stokes equations

Newton's second law of motion for a fluid element:



Navier-Stokes equations:

$$\rho \frac{D\underline{u}}{Dt} = \rho \underline{g} - \nabla p - \frac{2}{3} \nabla \left(\eta \nabla \cdot \underline{u} \right) + 2 \left(\nabla \cdot (\eta \nabla) \right) \underline{u} + \nabla \times \left(\eta (\nabla \times \underline{u}) \right)$$

■ 4 unknowns: *u*, *v*, *w*, *p*; 3 equations + the continuity equation

Continuity equation

Flux is a mass of fluid flowing per unit time through a unit area:

$$\underline{q} = \rho \underline{u}$$

Conservation of mass: outflow of mass from a volume equals to decrease of mass within the volume (integral form):

$$\frac{dm}{dt} + \bigoplus_{S} (\underline{q} \cdot \underline{n}) \, dS = 0$$

The divergence theorem:

$$\iint_{S} (\underline{q} \cdot \underline{n}) \, dS = \iiint_{V} (\nabla \cdot \underline{q}) \, dV$$

Differential form of continuity equation:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{u}) = 0$$

• If density ρ is constant: $\nabla \cdot \underline{u} = 0$

Towards the Reynolds equation

Introducing dimensionless variables:

$$X = \frac{x}{l_0}, \quad Y = \frac{y}{b_0}, \quad Z = \frac{z}{h_0}, \quad T = \frac{t}{t_0}, \quad \bar{u} = \frac{u}{u_0}$$

$$\bar{v} = \frac{v}{v_0}, \quad \bar{w} = \frac{w}{w_0}, \quad \bar{\rho} = \frac{\rho}{\rho_0}, \quad \bar{\eta} = \frac{\eta}{\eta_0}, \quad P = \frac{h_0^2 p}{\eta_0 u_0 l_0}$$

Reynolds number:

$$\mathcal{R} = \frac{\text{Inertia}}{\text{Viscous}} = \frac{\rho_0 u_0 l_0}{\eta_0}$$

• Thin fluid film: $h_0 \ll l_0$, $\mathcal{R} \ll 1$

$$\frac{\partial p}{\partial x} = \frac{\partial}{\partial z} \left(\frac{\partial u}{\partial z} \right)$$
$$\frac{\partial p}{\partial y} = \frac{\partial}{\partial z} \left(\frac{\partial v}{\partial z} \right)$$
$$\frac{\partial p}{\partial z} = 0 \rightarrow p = p(x, y)$$

Velocity profile



Calculating flow rates

$$u = \frac{\partial p}{\partial x} \frac{z^2 - zh}{2\eta} + u_1 \frac{z}{h} + u_2 \left(1 - \frac{z}{h}\right)$$
$$v = \frac{\partial p}{\partial y} \frac{z^2 - zh}{2\eta} + v_1 \frac{z}{h} + v_2 \left(1 - \frac{z}{h}\right)$$

Flow rate per unit width in x and y directions:

$$q'_x = \int_0^h u dz = -\frac{h^3}{12\eta} \frac{\partial p}{\partial x} + \frac{u_1 + u_2}{2}h$$
$$q'_y = \int_0^h v dz = -\frac{h^3}{12\eta} \frac{\partial p}{\partial y} + \frac{v_1 + v_2}{2}h$$

Integrating continuity equation across film thickness:

$$\int_{0}^{h} \left[\frac{\partial \rho}{\partial t} + \nabla \cdot \underline{u} \right] dz = 0$$

Reynolds equation

General form in 3D:

$$\frac{\partial}{\partial x} \left(\frac{\rho h^3}{12\eta} \frac{\partial p}{\partial x} \right) + \frac{\partial}{\partial y} \left(\frac{\rho h^3}{12\eta} \frac{\partial p}{\partial y} \right) = \frac{(u_1 + u_2)}{2} \frac{\partial(\rho h)}{\partial x} + \frac{(v_1 + v_2)}{2} \frac{\partial(\rho h)}{\partial y} + h \frac{\partial \rho}{\partial t}$$

If ρ , η are constant:

$$\frac{1}{12\eta}\frac{\partial}{\partial x}\left(h^{3}\frac{\partial p}{\partial x}\right) + \frac{1}{12\eta}\frac{\partial}{\partial y}\left(h^{3}\frac{\partial p}{\partial y}\right) = \frac{(u_{1}+u_{2})}{2}\frac{\partial h}{\partial x} + \frac{(v_{1}+v_{2})}{2}\frac{\partial h}{\partial y}$$

In 2D:

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial p}{\partial x} \right) = 6\eta (u_1 + u_2) \frac{\partial h}{\partial x}$$



O. Reynolds (1886)

Physically relevant models

Non-Newtonian fluid:

$$\eta = f\left(\frac{du}{dz}\right)$$

Viscosity-pressure dependency: Barus law

$$\eta(p) = \eta_0 e^{\alpha p}$$

Fluid compressibility:

$$K = -V \frac{dp}{dV} = \rho \frac{dp}{d\rho}$$
$$\rho = \rho_0 e^{(p-p_0)/K}$$

 Cavitation: process of bubble generation due to local pressure decline below saturated vapor pressure

Step slider bearing

Reynolds equation (ρ = const, η = const):

$$\frac{d}{dx}\left(h^3\frac{dp}{dx}\right) = 6u\eta\frac{dh}{dx}$$

Constant film thickness in both sections:

$$h(x) = \begin{cases} h_0 + s & 0 < x < nl \\ h_0 & nl < x < l \end{cases}$$
$$\frac{d^2 p}{dx^2} = 0, \quad x \in (0; nl) \cup (nl; l)$$
$$\frac{dp}{dx} = const, \quad x \in (0; nl) \cup (nl; l)$$



Step slider bearing

• Continuity of pressure:

$$p|_{x=nl-0} = p|_{x=nl+0} = p_m$$

$$nl\left(\frac{dp}{dx}\right)_i = -(1-n)l\left(\frac{dp}{dx}\right)_o$$

Continuity of flow rate:

$$q_{x,i}' = q_{x,o}'$$

$$\frac{(h_0+s)^3}{12\eta} \left(\frac{dp}{dx}\right)_i + \frac{u(h_0+s)}{2} = -\frac{h_0^3}{12\eta} \left(\frac{dp}{dx}\right)_o + \frac{uh_0}{2}$$

Maximum pressure:

$$p_m = 6\eta u l \left[\frac{n(1-n)s}{(1-n)(h_0+s)^3 + nh^3} \right]$$



Step slider bearing

Pressure distribution:

$$p(x) = \begin{cases} p_m \frac{x}{nl} & 0 < x < nl \\ p_m \frac{l - x}{(1 - n)l} & nl < x < l \end{cases}$$

$$p_m = 6\eta u l \left[\frac{n(1-n)s}{(1-n)(h_0+s)^3 + nh^3} \right]$$

 Optimal bearing configuration to produce the largest *p_m*:

$$\frac{\partial p_m}{\partial n} = 0 \quad \text{and} \quad \frac{\partial p_m}{\partial s} = 0$$

$$\begin{cases} (1-n)^2(h_0+s)^3 - n^2h_0^3 = 0\\ (1-n)(h_0+s)^2(h_0-2s) + nh_0^3 = 0 \end{cases}$$

Optimal values:

$$\frac{h_0}{s} = 1.155, \quad n = 0.7182$$



Inclined slider bearing

Reynolds equation (ρ = const, η = const):

$$\frac{d}{dx}\left(h^3\frac{dp}{dx}\right) = 6u\eta\frac{dh}{dx}$$

Integrating:

$$h^3 \frac{dp}{dx} = 6u\eta h + C$$

$$\frac{dp}{dx} = 0 \rightarrow h = h_m \Longrightarrow C = 6u\eta h_m$$
$$\frac{dp}{dx} = 6\eta u \left(\frac{h - h_m}{h^3}\right)$$
$$h(x) = h_0 + s \left(1 - \frac{x}{l}\right)$$

Introducing dimensionless variables:

$$X = \frac{x}{l}, \quad H = \frac{h}{s}, \quad H_m = \frac{h_m}{s}, \quad H_0 = \frac{h_0}{s} \Longrightarrow \quad P = \frac{ps^2}{\eta u l}$$



Inclined slider bearing

Dimensionless Reynolds equation:

$$\frac{dP}{dX} = 6\left(\frac{H - H_m}{H^3}\right)$$
$$H = H_0 + 1 - X, \quad \frac{dH}{dX} = -1$$

Integrating:

$$P = 6 \int \left(\frac{1}{H^2} - \frac{H_m}{H^3}\right) dX = 6 \left(\frac{1}{H} - \frac{H_m}{2H^2}\right) + C$$

BCs:

$$P = 0 \text{ when } X = 0 \to H = H_0 + 1$$

$$P = 0 \text{ when } X = 1 \to H = H_0$$

$$H_m = \frac{2H_0(1 + H_0)}{1 + 2H_0}, \quad C = -\frac{6}{1 + 2H_0}$$

$$P(X) = \frac{6X(1 - X)}{(H_0 + 1 - X)^2(1 + 2H_0)}$$





Inclined slider bearing

Dimensionless pressure distribution:

$$P(X) = \frac{6X(1-X)}{(H_0 + 1 - X)^2(1 + 2H_0)}$$

Dimensionless coordinate of maximum:

$$X_m = \frac{1 + H_0}{1 + 2H_0}$$

Dimensionless maximal pressure:

$$P_m = \frac{3}{2H_0(1+H_0)(1+2H_0)}$$

Dimensional maximal pressure:

$$p=P\frac{\eta ul}{s^2},\quad p_m=\frac{3\eta uls}{2h_0(s+h_0)(s+2h_0)}$$

• Optimal shoulder height: $\partial p_m / \partial s = 0 \rightarrow s_{opt} = \sqrt{2}h_0$





Elastohydrodynamic lubrication (EHL)

- Non-conforming surfaces
- Elastic deflection of solid walls
- Viscosity-pressure dependence: $\eta(p) = \eta_0 \exp \xi p$
- Hard EHL (metal parts):
 - $\begin{array}{l} 0.5 \; \mathrm{GPa} \leq p \leq 3 \; \mathrm{GPa} \\ 0.1 \; \mu\mathrm{m} \leq h_{\mathrm{min}} \leq 1 \; \mu\mathrm{m} \end{array}$
 - gears
 - rolling bearings
 - cams
- Soft EHL (polymer):
 - $p \approx 1 \text{ MPa}$
 - $h_{\min} \approx 1 \ \mu m$
 - seals
 - human joints
 - tires



Needle roller bearing www.farazbearing.com



Bevel gear www.linngear.com

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O-ring seal www.ecosealthailand.com

Elastohydrodynamic lubrication (EHL)

Reynolds equation:

$$\frac{d}{dx}\left(\frac{h^3}{\eta}\frac{dp}{dx}\right) = 12u\frac{dh}{dx}$$

 Viscosity-pressure dependence (Barus law):

 $\eta(p) = \eta_0 \, e^{\xi p}$

Film shape:

$$h(x) = h_0 + S(x) + \delta(x)$$

$$h_0 \quad \text{constant}$$

$$S(x) = \frac{x^2}{2R} \quad \text{undeformed geometry}$$

$$\delta(x) \quad \text{elastic deformation}$$

Contact constraints:

$$\begin{cases} h_0 + S(x) + \delta(x) = 0, & p > 0 \\ h_0 + S(x) + \delta(x) > 0, & p = 0 \end{cases}$$

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[1] D. Dowson, Wear (1995)

[2] B.J. Hamrock, "Fundamental of fluid film lubrication"" (1991) 19/33

EHL film thickness: experimental observation

- Ball-on-disk optical tribometer
- Measurement based on light interference principle
- Unidirectional start-stop-start motion
- Important for study of rolling contact fatigue and wear



Ball-on-disk apparatus with interferometry^[2]

[2] D. Kostal et al, Journal of Tribology (2017)



[1] P. Sperka et al, Journal of Tribology (2014)

EHL film thickness: experimental observation



Left to right: snapshots of interferograms, film thickness contour maps, results of numerical simulation^[1]

[1] P. Sperka et al, Journal of Tribology (2014)



direction^[1]

Lubrication regimes: Stribeck curve



Boundary lubrication

- Asperities come in contact
- $1 \text{ nm} \le h_{\min} \le 10 \text{ nm}$
- Bulk lubricant properties (i.e. viscosity) are not important
- Physical and chemical properties of the surface and of the fluid film are important
- Lubricant film of molecular size^[1]
- Breakdown of lubricant film at localized regions^[2], frictional force:

$$F = A \left(\alpha s_m + (1 - \alpha) s_l \right)$$

- *A* the area that supports the load
- α fraction of breakdown area
- s_m shear stress in solid contact
- s_l shear stress in the lubricating film

Therefore, if α - const, then $F \propto A$.

Shvarts & Yastrebov



The frictional resistance is due to interaction between the outer surfaces of the adsorbed monolayers without any solid contact occurring^[1] [1] W.B. Hardy (1936)



Mechanism involving breakdown of the lubricant film at small localized regions^[2] [1] F.P. Bowden and D. Tabor, "The friction and Lubrication of Solids (1950)

Mixed (partial) lubrication

- Combination of boundary and fluid film effects
- Some asperity contact
- Film layer of one or more molecular layers
- Smooth transition
- $0.01 \ \mu m \le h_{\min} \le 1 \ \mu m$

Lubrication: friction coefficient and wear



Lubrication: take home messages

- Lubrication: reduction of wear and friction between relatively moving surfaces by adding lubricant
- Hydrodynamic: full separation of solids, thin fluid film lubrication (Reynolds equation), dynamic viscosity is important
- EHL: solids deform elastically (hard metals, soft polymers), affected by viscosity-pressure dependence
- Boundary: contact of asperities, but still thin molecular level of lubricant, chemical properties important, breakdown of fluid film
- Mixed (partial): smooth transition
- Recommended literature:
 - **1** B.J. Hamrock et al, "Fundamentals of fluid film lubrication" (2004)
 - 2 F.P. Bowden and D. Tabor, "The friction and Lubrication of Solids (1950)
 - D. Dowson, "Elastohydrodynamic and micro-elastohydrodynamic lubrication", Wear, 190 (1995)

Sealing: what is it?

- Sealing: technique to prevent or reduce leakage of fluid from one chamber to another using seals
- Different types:
 - face seals
 - O-ring seals
 - labyrinth seals
- Dynamic/static
- Material: polymer/metallic
- Operate in EHL/mixed/boundary regimes





O-ring

Application: metal-to-metal static face seal

- Metal-to-metal static face seals used in fluid system of nuclear power plants
- Coting of the seal is made of material Norem^[1]: elasto-plastic Elastic moduli:

$$E = 175 \,\text{GPa}, \nu = 0.3$$

Yield stress:

$$\sigma_Y = R_0 + Q(1 - e^{-bp})$$

 $R_0 = 442.7 \text{ MPa}$ Q = 493.5 MPab = 242.2

J. Durand, PhD thesis (2012)









A A A external load



↑ ↑ ↑ ↑ ↑ external load

Surface discretization	Total DOFs	RAM	Cores	Time
256 × 256	1.4M	30 Gb	8	2-4 days
512 × 512	5.7M	140 Gb	16	4-8 days

Mechanical contact (unilateral):

$$\begin{array}{l} \nabla \cdot \underline{\underline{\sigma}}(\underline{u}) = 0 & \text{in } \Omega_s, \\ g(\underline{u}) \ge 0, \ \sigma_n(\underline{u}) \le 0, \ g(\underline{u}) \ \sigma_n(\underline{u}) = 0 & \text{at } \Gamma_c, \\ u_x|_{x=0,\lambda/2} = 0, & u_y|_{y=0,L} = 0, \end{array}$$

■ Thin fluid flow with immobile walls (Reynolds equation):

$$\begin{aligned} \nabla \cdot \left[g(\underline{u})^3 \nabla p_f \right] &= 0 & \text{in } \Gamma_f \\ p_f \Big|_{y=0} &= p_i, \quad p_f \Big|_{y=L} &= p_o \\ \left[\nabla p_f \cdot \underline{e}_x \right] \Big|_{x=0,\lambda/2} &= 0, \end{aligned}$$

Fluid/structure interface:

$$\sigma_n(\underline{\boldsymbol{u}}) = -\boldsymbol{p}_f \quad \text{at } \Gamma_f$$







Intensity of the fluid flux



Morphology of the contact interface



Intensity of the fluid flux



Morphology of the contact interface



Intensity of the fluid flux



Morphology of the contact interface



Intensity of the fluid flux



Distribution of the fluid pressure



Distribution of the free volume



Distribution of the fluid pressure



Distribution of the free volume



Distribution of the fluid pressure



Distribution of the free volume



Distribution of the fluid pressure



Distribution of the free volume



Distribution of the fluid pressure



Distribution of the free volume

Transmissivity of the interface



Transmissivity of the interface







FE mesh













Thank you for your attention!